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(12) **United States Patent**
Guan(10) **Patent No.:** **US 9,169,376 B2**
(45) **Date of Patent:** **Oct. 27, 2015**(54) **CHITIN NANOWHISKER COMPOSITES AND METHODS**(71) Applicant: **Qi Guan**, Scarborough (CA)(72) Inventor: **Qi Guan**, Scarborough (CA)(73) Assignee: **Boco Technology Inc.**, Toronto (CA)

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C08L 69/00 (2013.01)(58) **Field of Classification Search**

CPC C08B 37/003

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Primary Examiner — Wenwen Cai(74) *Attorney, Agent, or Firm* — Gilbert's LLP; Matthew D. Powell(57) **ABSTRACT**

A composite includes particles of thermoplastic polymer coated with a chitin nanowhisiker gel and melt-blended. The thermoplastic polymer may be polystyrene, polyethylene, acrylonitrile butadiene styrene, polycarbonate, or another thermoplastic polymer. A method of processing chitin includes forming a non-colloidal mixture substantially of chitin and hydrochloric acid to subject the chitin to hydrolysis; upon the mixture becoming substantially colloidal, controlling conditions of the mixture to slow the hydrolysis; dialyzing the substantially colloidal mixture to produce a processed colloidal mixture consisting substantially of water and crystalline chitin; and reducing amount of agglomerated crystalline chitin and water in the processed colloidal mixture thereby to yield chitin nanowhisiker gel. A method of forming a composite of chitin nanowhiskers dispersed in a thermoplastic polymer matrix includes coating thermoplastic polymer particles with a chitin nanowhisiker gel; and subjecting the coated particles to melt-blending thereby to form the composite.

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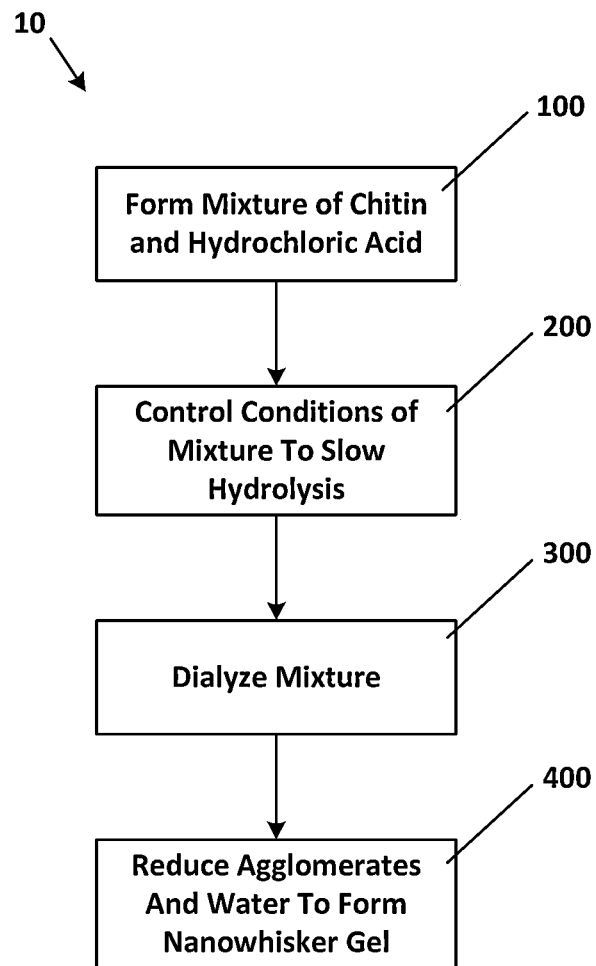


FIG. 1

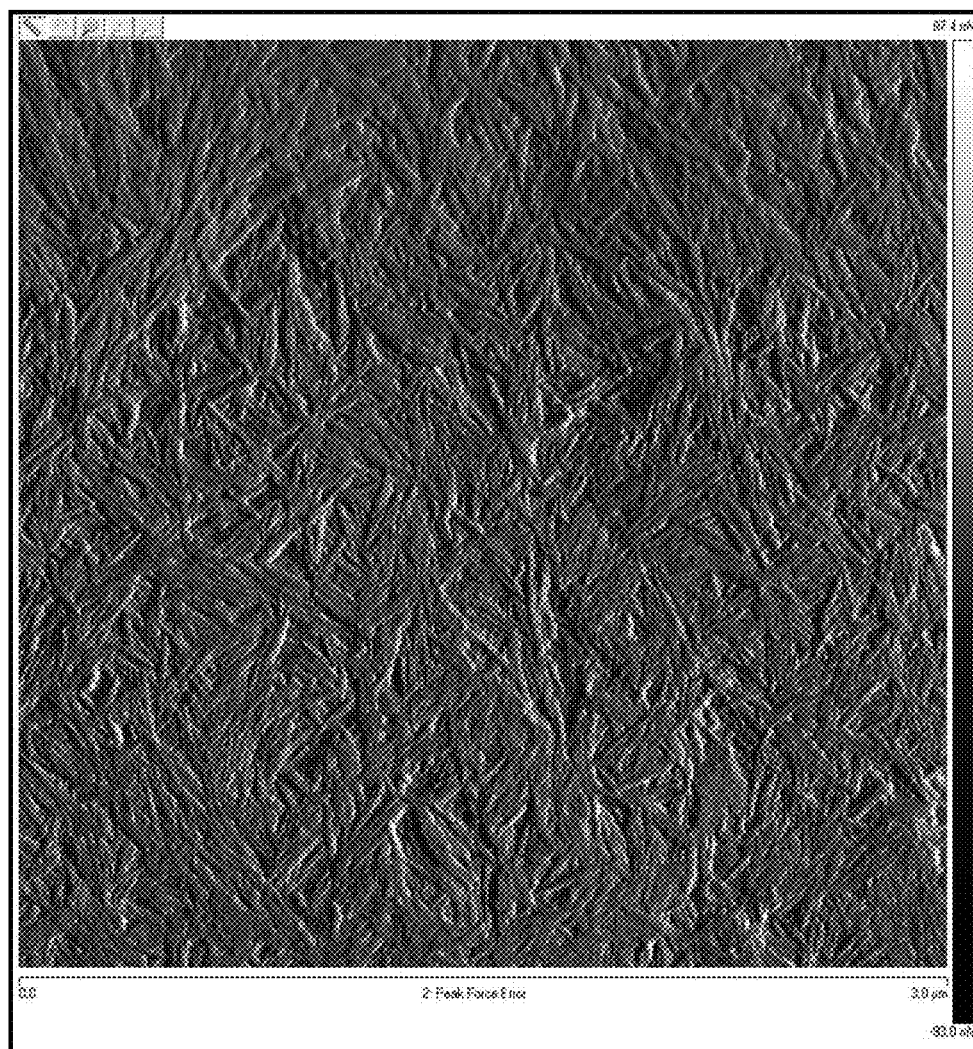


FIG. 2

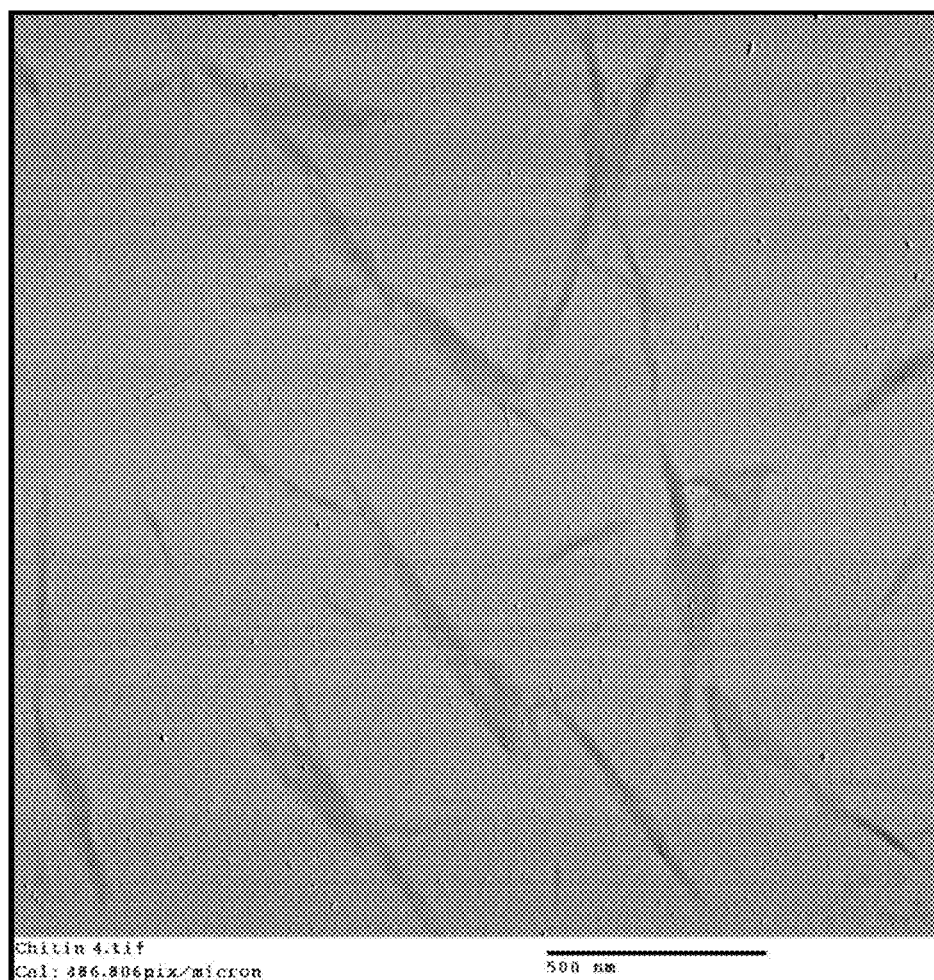


FIG. 3

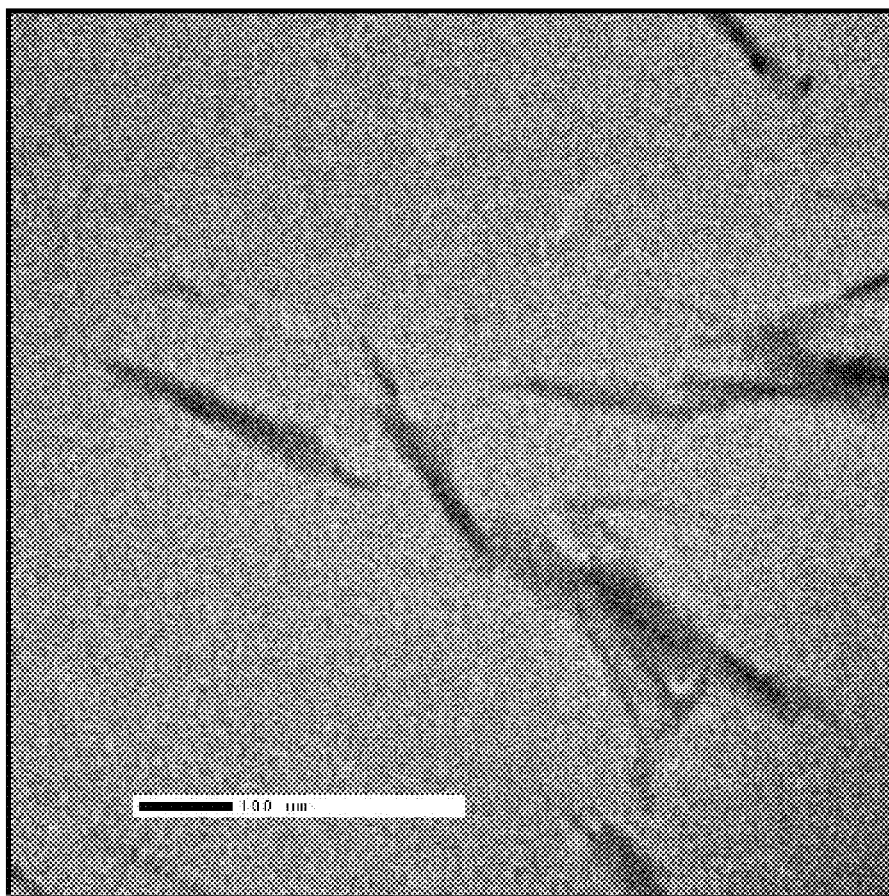


FIG. 4

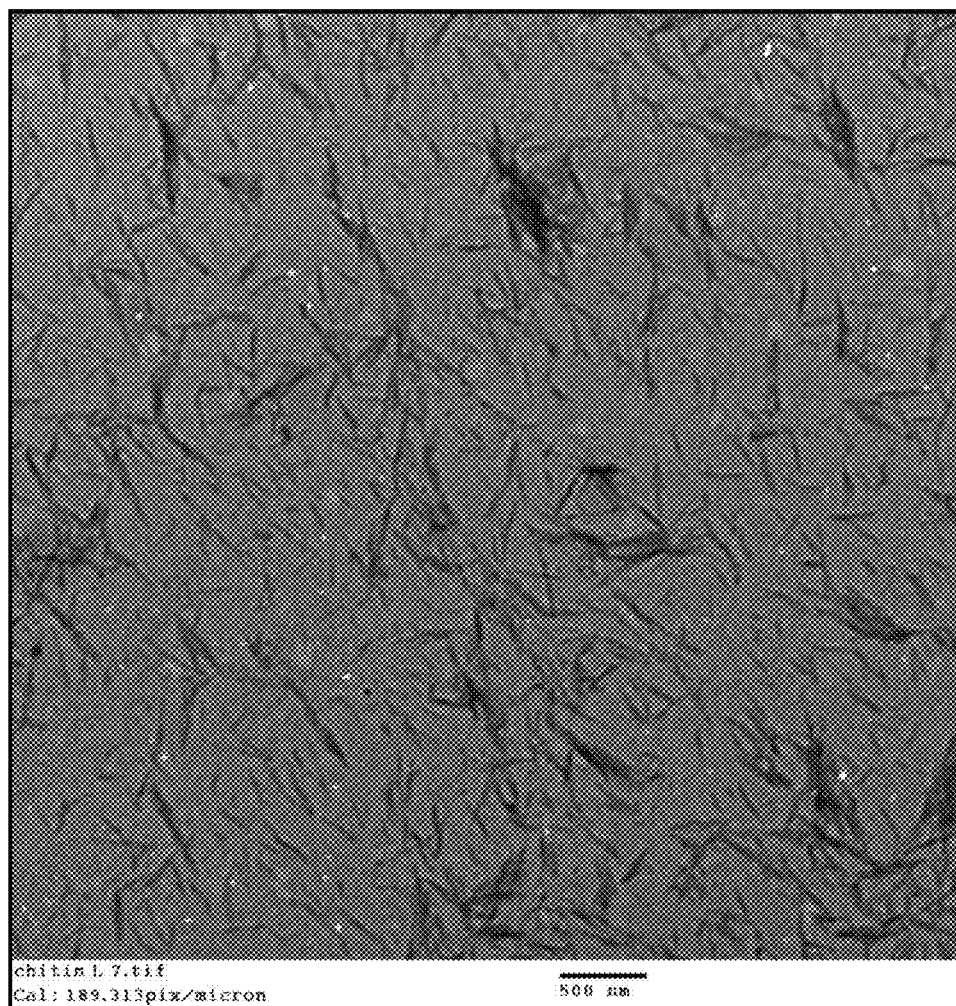
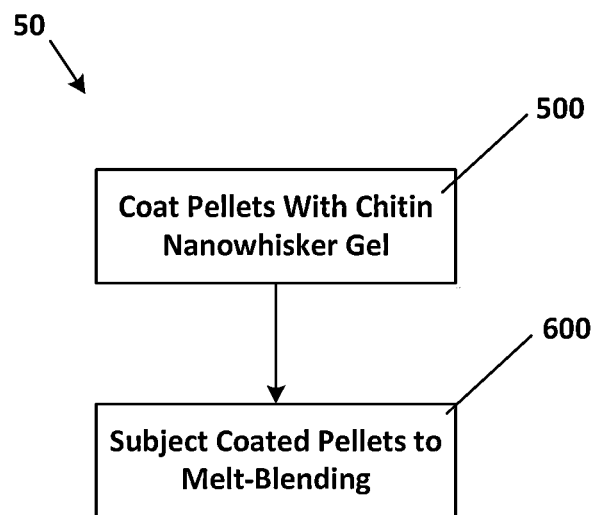


FIG. 5

**FIG. 6**

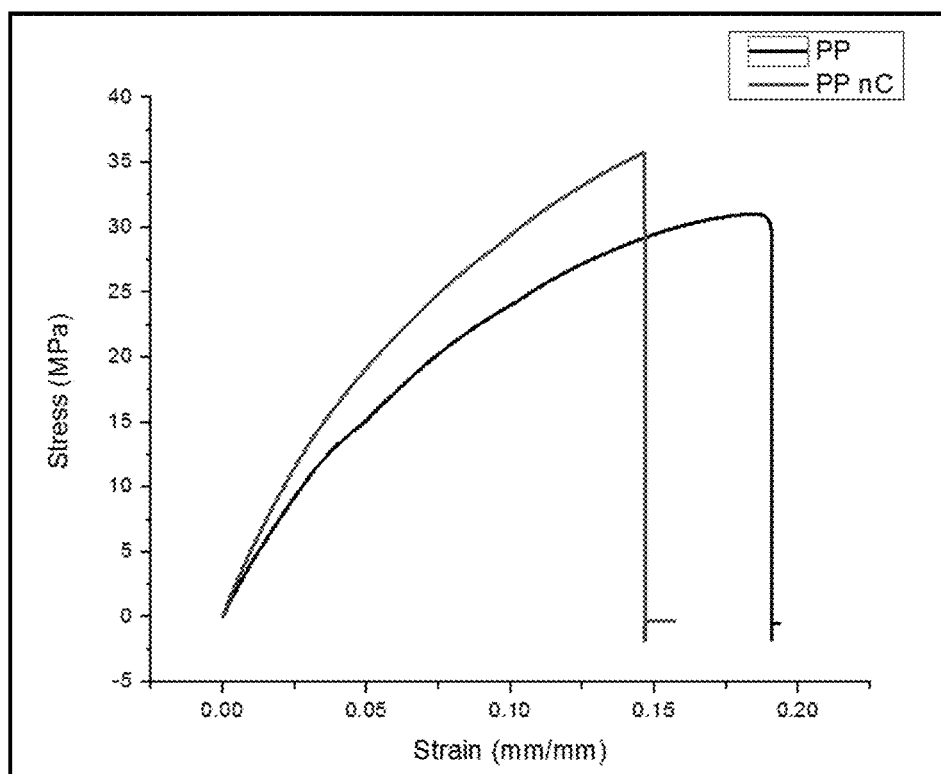


FIG. 7

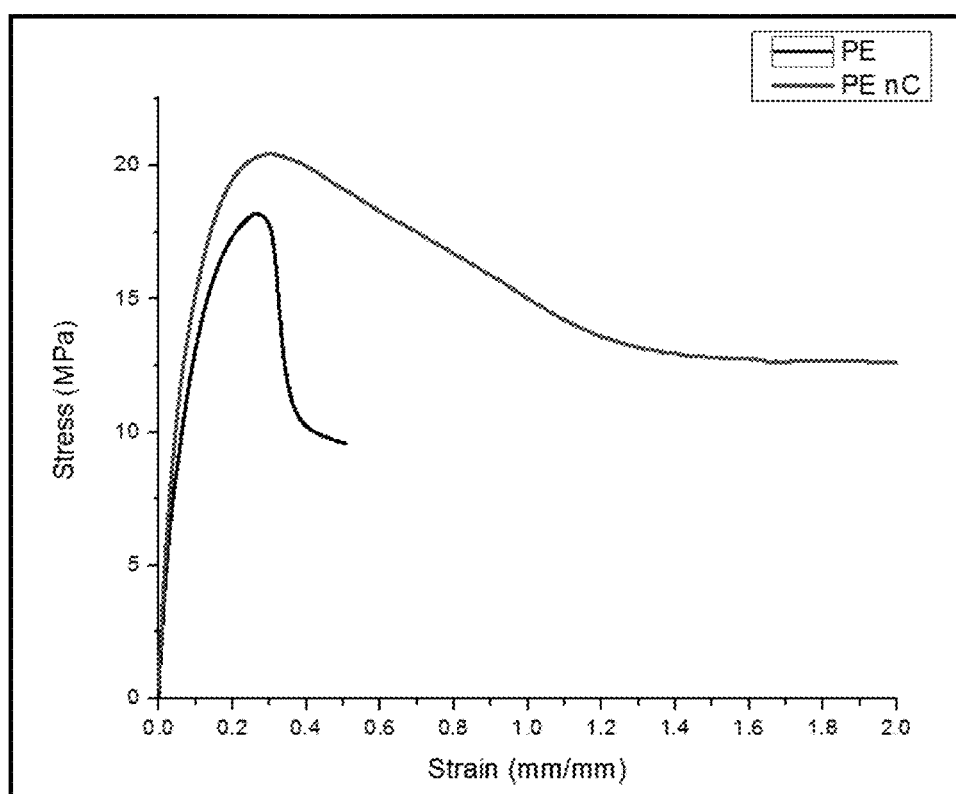


FIG. 8

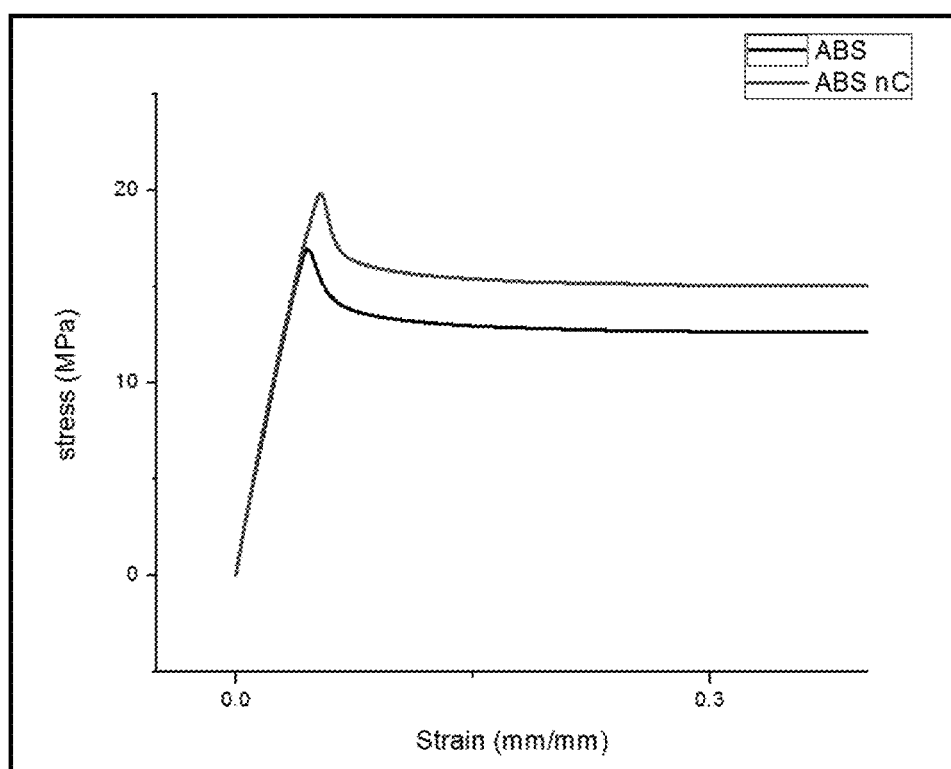


FIG. 9

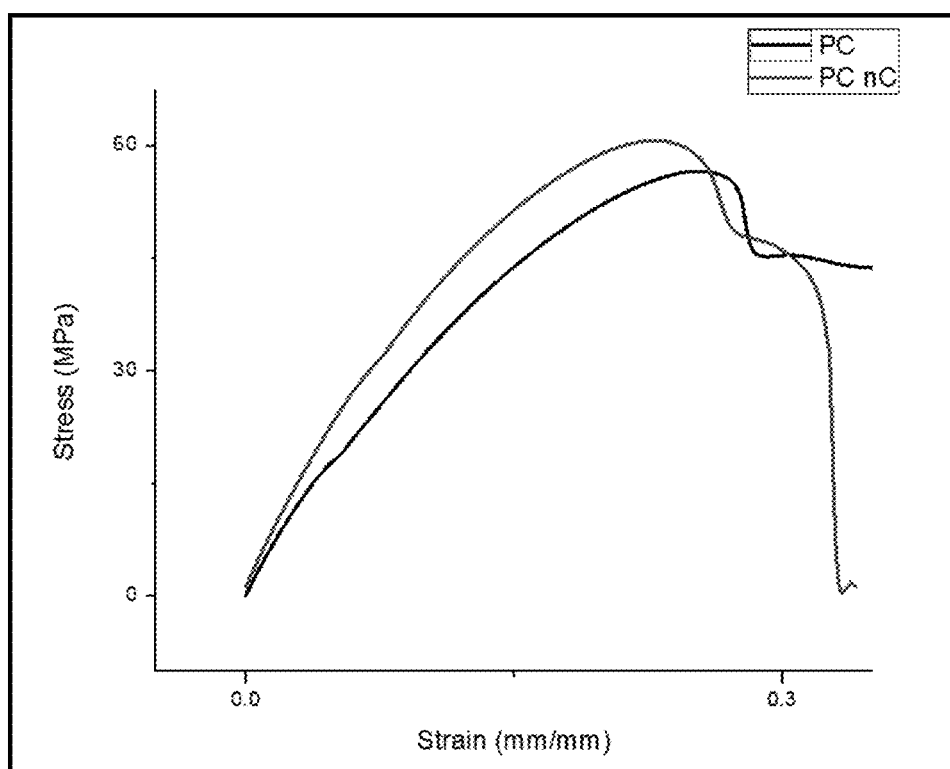


FIG. 10

CHITIN NANOWHISKER COMPOSITES AND METHODS

FIELD OF THE INVENTION

The following relates generally to nanocomposites and more particularly to chitin nanowhisker composites, methods of fabricating chitin nanowhisker composites, and methods of processing chitin.

BACKGROUND OF THE INVENTION

Nanoparticles are particles having one or more dimensions between 1 and 100 nanometers (nm). Due primarily to a high percentage of their atoms being positioned at the surface providing a very large surface area for their size, nanoparticles of a given material can exhibit markedly different properties and behaviours than larger particles of the same material.

Nanocomposites are multiple-phase materials, found in nature or fabricated, where one of the phases is nanoparticles. For example, a solid nanocomposite comprises nanoparticles dispersed in a bulk solid matrix. Due to the unique physical properties of nanoparticles, a small percentage of nanoparticles can have noticeable, macro-scale effects on the bulk solid matrix. As such, fabrication of nanocomposites having nanoparticles for imparting beneficial macro-scale mechanical, electrical, optical, dielectrical, thermal, antimicrobial or other effects is of great interest.

Nanofibrils, or nanowhiskers, are nanoparticles having a crystalline rod-like structure. Chitin nanowhiskers include crystalline polysaccharides having a diameter of about 10 nm and a length of about 200 nm to about 500 nm that may be found in an abundant, biodegradable and non-toxic structural polysaccharide material found in crustaceans such as shrimp and crab, known as chitin. Chitin nanowhiskers are desirable for nanocomposites due to their ability to impart desirable mechanical and antimicrobial effects, as well as due to their biodegradability, their abundance and their non-toxicity.

In nature, chitin contains both amorphous and crystalline chitin along with various other components such as proteins and the like. For forming nanocomposites, it is desirable to extract mostly individual chitin nanowhiskers from chitin so that the individual nanowhiskers can be dispersed throughout a bulk matrix. As such, it is desirable to process the chitin to generally extract only individual chitin nanowhiskers, without also extracting agglomerated chitin nanowhiskers that can be undesirably larger in size, amorphous chitin, and the proteins or other materials.

When forming the nanocomposites on an industrial scale using chitin nanowhiskers, it can be challenging to ensure that nanoparticles are generally uniformly dispersed in the bulk solid matrix. Unless the chitin nanowhiskers are dispersed in this way, an overall body of nanocomposite material will not exhibit the desirable properties uniformly. Too low a concentration of chitin nanowhiskers will have little beneficial effect, while too high a concentration of chitin nanowhiskers can undesirably weaken the material locally. Furthermore, if the overall body of nanocomposite material is to be subdivided into pellets or other smaller units prior to provision to a downstream process, there can be a wide variation in amounts of chitin nanowhiskers across individual pellets.

SUMMARY OF THE INVENTION

According to an aspect, there is provided a composite comprising particles of thermoplastic polymer coated with a chitin nanowhisker gel and melt-blended.

In an embodiment, the thermoplastic polymer comprises polypropylene. In another embodiment, the thermoplastic polymer comprises polyethylene. In another embodiment, the thermoplastic polymer comprises acrylonitrile butadiene styrene. In another embodiment, the thermoplastic polymer comprises polycarbonate. In another embodiment, the composite comprises various thermoplastic polymers.

According to another aspect, there is provided a composite comprising chitin nanowhiskers dispersed in polypropylene.

According to another aspect, there is provided a composite comprising chitin nanowhiskers dispersed in polyethylene.

According to another aspect, there is provided a composite comprising chitin nanowhiskers dispersed in acrylonitrile butadiene styrene.

According to another aspect, there is provided a composite comprising chitin nanowhiskers dispersed in polycarbonate.

According to another aspect, there is provided a method of processing chitin comprising forming a non-colloidal mixture substantially of chitin and hydrochloric acid to subject the chitin to hydrolysis; upon the mixture becoming substantially colloidal, controlling conditions of the mixture to slow the hydrolysis; dialyzing the substantially colloidal mixture to produce a processed colloidal mixture consisting substantially of water and crystalline chitin; and reducing amount of agglomerated crystalline chitin and water in the processed mixture thereby to yield chitin nanowhisker gel.

The method may further comprise freeze-drying the chitin nanowhisker gel thereby to yield substantially dry chitin nanowhiskers.

According to another aspect, there is provided a method of forming a composite of chitin nanowhiskers dispersed in a thermoplastic polymer matrix, the method comprising coating thermoplastic polymer particles with a chitin nanowhisker gel; and subjecting the coated particles to melt-blending thereby to form the composite.

Other aspects may become apparent to the ordinary skilled reader upon review of the following.

BRIEF DESCRIPTION OF THE DRAWINGS

Embodiments of the invention will now be described with reference to the appended drawings in which:

FIG. 1 is a flowchart showing steps in a method for processing chitin;

FIG. 2 is an image captured, using an atomic force microscope (AFM) using peak force error mode, of chitin nanowhiskers, wherein the scale bar is included within the image;

FIG. 3 is an image captured, using a transmission electron microscope (TEM), of chitin nanowhiskers;

FIG. 4 is another image captured, using a TEM, of chitin nanowhiskers;

FIG. 5 is another image captured, using a TEM, of chitin nanowhiskers;

FIG. 6 is a flowchart showing steps in a method of forming a composite including chitin nanowhiskers dispersed in a thermoplastic polymer matrix;

FIG. 7 is a graph showing a stress/strain curve for polypropylene (PP) and a counterpart PP-chitin nanowhisker composite (PP nC);

FIG. 8 is a graph showing a stress/strain curve for polyethylene (PE) and a counterpart PE-chitin nanowhisker composite (PE nC);

FIG. 9 is a graph showing a stress/strain curve for acrylonitrile butadiene styrene (ABS) and a counterpart ABS-chitin nanowhisker composite (ABS nC); and

FIG. 10 is a graph showing a stress/strain curve for polycarbonate (PC) and a counterpart PC-chitin nanowhis-
ker composite (PC nC).

DETAILED DESCRIPTION

Turning to FIG. 1, there is shown a flowchart with steps in a method 10 for processing chitin to yield a chitin nanowhis-
ker gel. An initially non-colloidal mixture substantially of
chitin and hydrochloric acid is first formed, to subject the
chitin to hydrolysis (step 100). In this embodiment, the chitin
introduced into the process is in powder form, hydrolysis is
conducted between about 80° C. (176° F.) and about 100° C.
(212° F.), and the HCl is between about 2.5N and about 4N.
The hydrolysis may be conducted at higher temperatures, but
at lower than the bottom end of this range hydrolysis tends not
to be effective.

While both crystalline and amorphous forms of the chitin
are chemically the same, they are structurally different
enough that the amorphous chitin is more reactive and there-
fore dissolves faster during acid hydrolysis than does the
crystalline chitin. This distinction enables the crystalline
form of chitin to withstand dissolution somewhat longer dur-
ing acid hydrolysis than the amorphous chitin. After a time,
which will depend on a number of factors including volumes
but may be between about 1 hour and about 4 hours, the
mixture will become substantially colloidal with the crystal-
line chitin dispersed and the amorphous chitin having been
dissolved. When the mixture reaches this substantially col-
loidal state, conditions of the mixture are controlled to rapidly
slow or stop the hydrolysis (step 200). This intervention is for
limiting the extent to which the crystalline chitin is itself
dissolved, so as to preserve crystalline chitin.

In this embodiment, controlling the conditions of the sub-
stantially colloidal mixture include both adding an amount of
a base such as sodium hydroxide (NaOH) to bring the HCl to
below 2.5N, and applying a chill to the substantially colloidal
mixture. Preferably, in order for the process to be carried out
safely on an industrial scale, the amount of sodium hydroxide
added to the substantially colloidal mixture is less than would
be required to cause a violent reaction with the hydrochloric
acid. However, lower amounts of sodium hydroxide will limit
the rate at which hydrolysis can be slowed or stopped. As
such, applying the chill to bring the temperature down rapidly
to a temperature at which hydrolysis is significantly slowed or
stopped, for example to below 25° C. (77° F.), along with the
adding of the base acts in combination to rapidly slow or stop
the hydrolysis. Alternatively, just chilling, chilling and dilut-
ing with water, or chilling, neutralizing and diluting with
water can be done. It will be understood that larger containers
will be required if diluting with water, which may be unde-
sirable when implementing the process on an industrial-scale.

With the conditions of the mixture having been controlled
to rapidly slow or stop the hydrolysis, the substantially col-
loidal mixture is then dialysed to produce a processed collo-
idal mixture consisting substantially of water and crystalline
chitin (step 300). The dialysis serves to remove constituents
of the mixture other than the water and the crystalline chitin.
Advantageously, adding sodium hydroxide to slow or stop
hydrolysis in the controlling step also puts the mixture in a
condition to increase the rate of dialysis itself, when com-
pared to dialysis with just the hydrochloric acid. In particular,
with the addition of sodium hydroxide (NaOH) to the hydro-
chloric acid (HCl), water and ions of sodium and chlorine
(Na⁺ and Cl⁻, respectively), are produced. As such, the
osmotic pressure during hydrolysis that is acting individually
on each of the Na⁺ and Cl⁻ ions and the residual HCl is, in

aggregate, greater than the osmotic pressure that would act
independently on individual particles of HCl were the base
not added. This increase in the rate of dialysis has the poten-
tial to increase the speed at which the process can be executed,
which carries advantages when implementing on an indus-
trial scale. In alternative embodiments, with the addition of a
different base, different by-products would result. However,
the osmotic pressure advantage would remain. Examples of
bases include potassium hydroxide, barium hydroxide,
cesium hydroxide, sodium hydroxide, strontium hydroxide,
calcium hydroxide, lithium hydroxide, and rubidium hydrox-
ide. Other bases may be used, and selection of a base may
involve consideration of factors such as the toxicity of the
by-products and the ease with which they may be disposed.

In this embodiment, dialysis is conducted using a cellulose
semi-permeable membrane having pores that permit egress of
HCl, Na⁺ and Cl⁻ without permitting egress of the chitin
nanowhiskers in the mixture. As is well known, in order to
avoid damaging a cellulose membrane, the temperature of the
mixture to be dialyzed should be lower than the about 80° C.
to about 100° C. temperature at which the hydrolysis is con-
ducted. As such, chilling during the controlling step serves
dual purposes of helping to stop or slow the hydrolysis as well
as putting the mixture into a condition for dialysis with the
cellulose membrane. The time for dialysis generally depends
on the osmotic pressure, so flushing of the opposite side of the
membrane may be done on a regular basis based on pH
measurements, in an effort to preserve high osmotic pressure
over the time dialysis is to be conducted. In an alternative
embodiment, osmotic pressure may be increased by applying
physical pressure to the mixture to force particles through the
membrane. Other semi-permeable membranes may be
employed for dialysis that either do not require cooling, or
that require more or less cooling than a cellulose semi-per-
meable membrane.

Pursuant to the dialysis, crystalline chitin will remain that
is likely to include agglomerated chitin nanowhiskers as well
as individual chitin nanowhiskers. Because large agglomera-
tions of chitin nanowhiskers generally do not impart the ben-
eficial effects for nanocomposites that are imparted by indi-
vidual chitin nanowhiskers or very small agglomerations of
chitin nanowhiskers, it is desirable to separate the individual
chitin nanowhiskers and very small agglomerations of chitin
nanowhiskers from the large agglomerations of nanowhis-
kers. As such, following step 300, the amount of agglomer-
ated chitin nanowhiskers in the processed colloidal mixture is
reduced, as is the amount of water, in order to yield the chitin
nanowhis-ker gel (step 400).

In this embodiment, during reducing the amount of
agglomerated chitin nanowhiskers, the processed colloidal
mixture resulting from dialysis is subjected to centrifuging.
Since the agglomerated chitin nanowhiskers desired to be
removed from the processed colloidal mixture are many times
heavier than the individual chitin nanowhiskers that are to
remain, the time and speed of centrifuging are controlled to
move the agglomerated chitin nanowhiskers out of the main
body of the processed colloidal mixture for disposal, without
also moving very much individual chitin nanowhiskers. Low
RPM is preferred for subjecting the individual chitin nano-
whiskers to less force, but there is a trade off with the time it
takes to move the agglomerated chitin nanowhiskers from the
processing colloidal mixture. Once this centrifuging is con-
ducted, the higher-viscosity layer containing the agglomer-
ated chitin nanowhiskers is separated off and disposed of or
routed elsewhere for further processing.

During reducing the amount of water, the processed col-
loidal mixture with agglomerated chitin nanowhiskers having

been removed is subjected to additional centrifuging under different conditions. The goal of this additional centrifuging is to concentrate the chitin nanowhiskers into a high-viscosity layer to produce a chitin nanowhisker gel and to separate off the lower-viscosity layer (substantially water) that contains no or very few chitin nanowhiskers for disposal or routing elsewhere for further processing. In this embodiment, the centrifuging yields a chitin nanowhisker gel that is about 20% chitin nanowhiskers and 80% water, by weight. Control is exercised to ensure the concentration of chitin nanowhiskers in the gel is not too great, because as the concentration of chitin nanowhiskers in the gel rises, the likelihood of agglomeration of the chitin nanowhiskers rises accordingly. As an alternative to, or in combination with, centrifuging, evaporation may be employed for reducing the amount of water.

Preferably the method is conducted on a continuous basis, rather than a batch basis, such that chitin is continuously being input into the process and chitin nanowhisker gel is continuously being yielded by the process. Conducting the method on a continuous basis makes it more amenable to industrial scale production of chitin nanowhisker gel. For example, machines for continuous centrifuging may be employed.

FIG. 2 is an image captured, using an atomic force microscope (AFM) using peak force error mode, of chitin nanowhiskers, wherein the scale bar is included within the image. FIGS. 3 through 5 are images captured, using a transmission electron microscope (TEM), of chitin nanowhiskers.

The chitin nanowhisker gel may be used for producing nanocomposites, or further processed to produce a chitin nanowhisker powder that itself may be used for producing nanocomposites. Preferably, such further processing to produce the chitin nanowhisker powder comprises lyophilising, or freeze-drying, the chitin nanowhisker gel. This is done in order to limit the extent to which the chitin nanowhiskers agglomerate with the loss of water, as compared with simply causing the water in the gel to evaporate. Without wishing to be bound to a particular theory, it is believed that evaporation permits individual chitin nanowhiskers to gradually organize into agglomerations, whereas the nature of freeze-drying limits such opportunities to produce fewer agglomerations.

The chitin nanowhisker gel may be employed in a downstream or separate process for producing nanocomposites having the chitin nanowhiskers dispersed in a bulk solid matrix such as a thermoplastic polymer. Turning to FIG. 6, a method 50 of forming a composite of chitin nanowhiskers dispersed in a thermoplastic polymer matrix is shown. During the method, thermoplastic polymer particles are coated with a chitin nanowhisker gel (step 500) and the coated particles are subjected to melt-blending thereby to form the composite (step 600).

Preferably the particles are pellets having a maximum diameter of about 1 centimeter (cm), and more preferably the majority of the pellets have a diameter of about 2 to about 3 millimeters (mm). The composite may be further processed for form pellets of composite, or further processed to powder form.

Generally, coating is conducted to position nanowhiskers suspended in the gel with respect to the thermoplastic particles so as to facilitate dispersion of the nanowhiskers throughout the melted or softened thermoplastic polymer upon melt-blending. This technique makes it much more likely that a composite will be produced that has more uniform nanowhisker dispersion than those composites produced by methods that merely layer chitin nanowhisker gel atop a layer of the thermoplastic particles just prior to melt-blending. For example, with the prior layering methods, a

great number of adjacent thermoplastic particles may not be in contact with, or even physically near to, the nanowhisker gel at the time of melt-blending, and a great volume of nanowhiskers gel may not be in contact with, or even physically near, the thermoplastic particles. In such cases, upon melt-blending sections of thermoplastic matrix can be formed that incorporate too few or too many chitin nanowhiskers, causing uniformity of the nanocomposite to suffer. In particular, sections of the nanocomposite can be formed that do not exhibit the beneficial properties that are desired of the nanocomposite as a whole, despite the correct overall relative amounts of matrix and nanowhiskers.

Furthermore, as the melt-blending involves evaporation of the dispersion medium of the nanowhisker gel, insufficiently coating the particles with nanowhisker gel can result in agglomerations of chitin nanowhiskers rather than dispersion of individual chitin nanowhiskers in the thermoplastic polymer matrix.

Two primary factors determine the viability of the thermoplastic polymer being chosen for the matrix. The first is that, at least where the dispersion medium of the chitin nanowhisker suspension is water, the thermoplastic polymer should have a relatively low melting point at or below about 200 degrees C. The water is useful as a polar liquid medium that keeps the chitin nanowhiskers separated so they can be well-dispersed during melt-blending in the thermoplastic matrix. Accordingly, blending of the chitin nanowhiskers with the thermoplastic polymer during the melt-blending should begin prior to complete evaporation of the water. It will be understood that, where the dispersion medium is not water and has properties that cause it to evaporate differently than a water dispersion medium, a thermoplastic polymer with an accordingly higher melting point may be chosen. Furthermore, the temperature at which melt-blending is done can be regulated to account for various melting temperatures and rates of dispersion medium evaporation, or concentration of water can be established so as to delay full evaporation.

The second factor determining the viability of the thermoplastic polymer being chosen for the matrix relates to water degrading certain thermoplastic polymers during the melt/blending process. For example, if water is the dispersion medium of the suspension, those thermoplastic polymers that are easily degraded by water may not be viable. If such water-degradable thermoplastic polymers are to be used, it may be prudent to choose a dispersion medium other than water that will not degrade the thermoplastic polymer. However, it should be borne in mind that, while water can trigger degradation of a given thermoplastic polymer, provided the reinforcement provided by the dispersed chitin nanowhiskers at least makes up for the degradation, the composition formed of that thermoplastic polymer is viable.

While it is preferred that each particle of thermoplastic polymer, whether pellet or powder, be individually coated simply for uniformity of mechanical properties across the entire body of the resultant nanocomposite, as a practical industrial matter not each and every particle must be completely coated in order for the overall body of the composite to benefit from the nanowhiskers.

Furthermore, melt-blending can be conducted under conditions that do not strictly "melt" the thermoplastic polymer, but sufficiently soften the thermoplastic polymer so that the chitin nanowhiskers can be dispersed.

The method of forming a composite described above may be employed to form a composite comprising particles of thermoplastic polymer coated with a chitin nanowhisker gel and melt-blended. The thermoplastic polymer may comprise polypropylene, polyethylene, acrylonitrile butadiene styrene,

polycarbonate or other suitable thermoplastic polymer. The composite may comprise about 1% wt to about 5% wt chitin nanowhiskers.

EXAMPLES

Composites including chitin nanowhiskers dispersed in various thermoplastic polymers were fabricated. In each case, fabrication generally included coating thermoplastic particles with a chitin nanowhisger gel and subjecting the coated particles to melt-blending thereby forming the composite. In this embodiment, the majority of the particles were pellets with a diameter of about 2-3 millimeters.

In these examples, the dispersion medium of the chitin nanowhisger gel was water, and the chitin nanowhisger gel was produced according to the method described above.

Polypropylene (PP), Polyethylene (PE), Acrylonitrile butadiene styrene (ABS), Polycarbonate (PC) were experimentally determined to be viable for composites along with chitin nanowhisger. For example, viable composites include: a composite comprising chitin nanowhiskers dispersed in polypropylene, a composite comprising chitin nanowhiskers dispersed in polyethylene, a composite comprising chitin nanowhiskers dispersed in acrylonitrile butadiene styrene, and a composite comprising chitin nanowhiskers dispersed in polycarbonate. Various other thermoplastic polymers satisfying the above two conditions are likely to be viable candidates. In one embodiment, melt-blending was conducted 15-20 degrees above the melting temperature of the thermoplastic polymer to be used. At 20% chitin concentration, the gel was 5-10% wt of the thermoplastic polymer pellets.

Compositions comprising about 1% wt chitin nanowhiskers compositions were fabricated as described above, and the fabricated compositions were subjected to tensile testing. In particular, tensile testing involved characterizing the tensile properties of the composites and foams on a tensile testing system (Instron Micro Tester 5848). The composition specimens were fabricated in accordance with ASTM D638 type 5 standard dogbone shape (7.62 mm gage length, 3 mm width, 1.5 mm thickness) and tensile tested with a strain rate of 0.5 mm/minute.

FIGS. 7 through 10 are graphs showing typical stress/strain curves, for respective ones of the above-described tests of PP, PE, ABS and PC alone and the respective 1% nanocomposite counterparts. All graphs represent test results as the average of four (4) samples. Typical stress/strain curves are presented.

Table 1 below summarizes the comparisons of Ultimate Tensile Strength (UTS), Modulus, and Elongation between PP and the corresponding nanocomposite (PP nC) as depicted in the graph of FIG. 7:

TABLE 1

	PP	PP nC
UTS	31.57 ± 0.61	34.17 ± 0.786
Modulus	363.29 ± 24.96	433.35 ± 34.23
Elongation	0.203 ± 0.015275	0.1707 ± 0.02269

Table 2 below summarizes the comparisons of Ultimate Tensile Strength (UTS), Modulus, and Elongation between PE and the corresponding nanocomposite (PE nC) as depicted in the graph of FIG. 8:

TABLE 2

	PE	PE nC
UTS	18.39 ± 0.955	20.31 ± 0.831
Modulus	248.17 ± 19.437	258.44 ± 16.474
Elongation	0.358 ± 0.054	3.03 ± 0.975

Table 3 below summarizes the comparisons of Ultimate Tensile Strength (UTS), Modulus, and Elongation between ABS and the corresponding nanocomposite (ABS nC) as depicted in the graph of FIG. 9:

TABLE 3

	ABS	ABS nC
UTS	17.81 ± 0.938	19.42 ± 0.366
Modulus	428.09 ± 16.02	440.61 ± 4.57
Elongation	0.45 ± 0.255	0.585 ± 0.0517

Table 4 below summarizes the comparisons of Ultimate Tensile Strength (UTS), Modulus, and Elongation between PC and the corresponding nanocomposite (PC nC) as depicted in the graph of FIG. 10:

TABLE 4

	PC	PC nC
UTS	57.06 ± 0.5416	59.12 ± 0.4588
Modulus	442.53 ± 14.79	494.85 ± 15.66
Elongation	0.4475 ± 0.166	0.3279 ± 0.0168

Although embodiments have been described with reference to the drawings, those of skill in the art will appreciate that variations and modifications may be made without departing from the spirit and scope thereof as defined by the appended claims.

What is claimed is:

1. A method of processing chitin comprising:

forming an initially non-colloidal mixture substantially of chitin and about 2.5N to about 4N hydrochloric acid to subject the chitin to hydrolysis;

upon the initially non-colloidal mixture becoming substantially colloidal, controlling conditions of the substantially colloidal mixture to slow the hydrolysis, wherein controlling conditions of the substantially colloidal mixture comprises, without substantially diluting the substantially colloidal mixture, adding a base to the substantially colloidal mixture and applying a chill to the substantially colloidal mixture to rapidly bring the substantially colloidal mixture to below about 25° C. (77° F.);

dialyzing the substantially colloidal mixture to produce a processed colloidal mixture consisting substantially of water and crystalline chitin; and
reducing amount of agglomerated crystalline chitin and water in the processed colloidal mixture thereby to yield chitin nanowhisger gel.

2. The method of claim 1, further comprising lyophilizing the chitin nanowhisger gel thereby to yield substantially dry chitin nanowhiskers.

3. The method of claim 1, wherein the base is selected from the group consisting of potassium hydroxide, barium hydroxide, cesium hydroxide, sodium hydroxide, strontium hydroxide, calcium hydroxide, lithium hydroxide, and rubidium hydroxide.

4. The method of claim 1, wherein the initially non-colloidal mixture becomes substantially colloidal when amorphous chitin dispersed in the initially non-colloidal mixture is below a threshold amount.

5. The method of claim 1, wherein adding the base to the mixture reduces the concentration of the hydrochloric acid to below 2.5N. 5

6. The method of claim 1, wherein the step of reducing amount of agglomerated crystalline chitin comprises subjecting the processed mixture to centrifuging. 10

7. The method of claim 1, wherein the step of reducing amount of water in the processed mixture comprises subjecting the processed mixture to centrifuging.

8. The method of claim 1, wherein the step of reducing amount of water in the processed mixture comprises subjecting the processed mixture to evaporation. 15

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